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## Optimization of Wood Vinegar from Cacao Pod Shells by Response Surface Methodology

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## RESEARCH ARTICLE

# Optimization of Wood Vinegar from Cacao Pod Shells by Response Surface Methodology

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## ABSTRACT

The purpose of this study is to find the optimal conditions for producing wood vinegar from cacao pod shells using Response Surface Methodology (RSM). Box Behnken Design (BBD) was used to optimize the variables of pyrolysis times, temperature, and particle size. Wood vinegar was prepared by slow pyrolysis technology. The RSM with three design variables including pyrolysis duration at 50, 75, and 100 minutes; pyrolysis temperatures at 300°C, 340°C, and 380°C; and particle size of 3, 5 and 7 cm with 15 runs were applied. Chemical characterization of wood vinegar was performed by Gas Chromatography-Mass Spectrometry (GC-MS) analysis. The results showed that phenolic, furan, and ketone compounds were the main component in the cacao pod shells vinegar. The optimum production of wood vinegar from cacao pod shells based on RSM results was identified at a pyrolysis time of 100 minutes, a temperature of 353°C, and a particle size of 3 cm.

**Keywords:** Cacao pod shells, Optimization, Pyrolysis, RSM, Wood vinegar

## Introduction

Indonesia is a tropical country with abundant natural resources, one of which is cacao. In the agricultural sub-sector, the production of cacao (*Theobroma Cacao. L*) is ranked the third in the world. Indonesia's cacao production reaches 700.000 tons.<sup>1</sup> Generally, cacao is used as the main raw material in the chocolate industry and its derivative products. The volume of chocolate production will always be in direct proportion to the amount of cacao pod shell waste produced. Cacao pod shells weigh between 52–76% of the total fruit weight. Only 10% of the cacao pod is utilized, leaving 90% of the pod discarded as waste.<sup>2</sup> Obtaining one ton of cacao beans will produce 10 tons of cacao pod shell waste.<sup>3</sup> The amount of waste generated can pollute the environment, causing

odor and disease. Cacao pod shells contain cellulose compounds 35%; hemicellulose 20%; and lignin 18.6%.<sup>4–6</sup> Several previous studies have used cacao pod shells as animal feed,<sup>7</sup> biogas<sup>8</sup> and fertilizer.<sup>9</sup> A previous study using cacao pod waste to produce wood vinegar using the pyrolysis method was carried out by Desvita et al.<sup>10</sup>

Wood vinegar has been widely produced using various raw materials from biomass waste such as durian rind,<sup>11</sup> coconut shell,<sup>12,13</sup> oil palm empty fruit bunches,<sup>14</sup> rubber tree bark,<sup>15</sup> rice husks,<sup>16,17</sup> and wood sawdust.<sup>18</sup> Several previous studies have characterized the wood vinegar from various biomass wastes, in addition to studying the factors that affect the production of wood vinegar including pyrolysis temperature, pyrolysis time, the particle size of biomass, and the type of biomass used. These factors

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**Table 1.** The variables selected for the BBD.

| Independent Variable  | Symbol | Coded variable |             |           |
|-----------------------|--------|----------------|-------------|-----------|
|                       |        | Low<br>–1      | Center<br>0 | High<br>1 |
| Pyrolysis time        | A      | 50             | 75          | 100       |
| Pyrolysis temperature | B      | 300            | 340         | 380       |
| Particle size         | C      | 3              | 5           | 7         |

affect the wood vinegar yield; therefore, optimization is necessary. Several researchers have conducted experiments on the variations in wood raw material particles, pyrolysis temperature, pyrolysis time, heating rate, and residence time of hot vapours.<sup>19,20</sup>

Response surface methodology is a set of statistical-based mathematical models to design research.<sup>21</sup> The method has been widely used in optimizing the factors that affect the production/yield. It is useful for modeling and studying the influence and interaction between independent variables to optimize the response variable.<sup>22</sup> In previous studies,<sup>23</sup> RSM has been used to maximize the production of wood vinegar from durian rinds by slow pyrolysis. Optimization of wood vinegar yield from *Acacia mangium* has also identified the pyrolysis variables that affect the optimal yield of wood vinegar by pyrolysis method, namely pyrolysis residence time, moisture content, and chimney inclination angle.<sup>21</sup> Oramahi et al.<sup>19</sup> employed RSM to investigate the effect of variables in pyrolysis of *Shorea laevis* Ridl Wood including pyrolysis time, pyrolysis temperature, and biomass particle size, resulting in the maximum yield of 30.31%. However, no studies have been carried out to optimize the wood vinegar production from cacao pod shells as a raw material. The purpose of this study was to find out the best conditions for optimized production of wood vinegar from cacao pod shells using RSM. The parameters used were pyrolysis time, pyrolysis temperature, and biomass particle size, which were optimized for the response variable of wood vinegar yield.

## Materials and methods

### Preparation of wood vinegar

Wood vinegar was prepared from burning cacao pod shells in a pyrolysis reactor. The procedures and methodology were carried out in the same way as the previous studies by Faisal et al.<sup>11</sup> First, cacao pod shells were dried in the sun ( $\pm 5$  days). Three kg of the dry cacao pod shells were put into a stainless-steel pyrolysis reactor (5 kg capacity, and 50 cm height  $\times$  32 cm diameter) and heated up to the targeted temperatures of 300°C, 340°C, and 380°C, with pyrolysis times of 50, 75 and 100 minutes, and particle size of 3, 5 and 7 cm, Table 1. To produce

**Table 2.** Components of wood vinegar at 300°C pyrolysis.<sup>10</sup>

| No. | Component                          | Area     | %      |
|-----|------------------------------------|----------|--------|
| 1   | Phenol                             | 27105257 | 45.493 |
| 2   | Butyrolactone                      | 9854621  | 16.54  |
| 3   | Phenol, 3-methyl-                  | 5544816  | 9.306  |
| 4   | Phenol, 2-methoxy-                 | 5075314  | 8.518  |
| 5   | Phenol, 2-methyl-                  | 2903600  | 4.873  |
| 6   | 2-Furanmethanol                    | 2818770  | 4.731  |
| 7   | Methenamine                        | 2713902  | 4.555  |
| 8   | 2-Cyclopenten-1-one, 2,3-dimethyl- | 2139887  | 3.592  |
| 9   | Heptane, 4-methyl-                 | 1424656  | 2.391  |

**Table 3.** Components of wood vinegar at 340°C pyrolysis.<sup>10</sup>

| No. | Component                             | Area     | %      |
|-----|---------------------------------------|----------|--------|
| 1   | Phenol                                | 33601237 | 29.784 |
| 2   | 2-Furanmethanol                       | 19213385 | 17.031 |
| 3   | Phenol, 2-methoxy-                    | 15857099 | 14.056 |
| 4   | Phenol, 3-methyl-                     | 9048916  | 8.021  |
| 5   | Butyrolactone                         | 6165691  | 5.465  |
| 6   | 2-Cyclopenten-1-one, 2,3-dimethyl-    | 5419011  | 4.803  |
| 7   | Ethanone, 1-(2-furanyl)-              | 4789650  | 4.246  |
| 8   | Phenol, 2-methyl-                     | 4628925  | 4.103  |
| 9   | Methenamine                           | 3414745  | 3.027  |
| 10  | Phenol, 4-ethyl-                      | 3168724  | 2.809  |
| 11  | 2-Aminopyridine                       | 2693033  | 2.387  |
| 12  | 2-Cyclopenten-1-one, 2-methyl-        | 1761855  | 1.562  |
| 13  | 1-Propanol, 2-amino-                  | 1624076  | 1.44   |
| 14  | 1-Butanol, 3-methyl-, carbonate (2:1) | 1429822  | 1.267  |

**Table 4.** Components of wood vinegar at 380°C pyrolysis.<sup>10</sup>

| No. | Component                          | Area     | %      |
|-----|------------------------------------|----------|--------|
| 1   | Phenol                             | 53394823 | 33.603 |
| 2   | 2-Furanmethanol                    | 21037840 | 13.24  |
| 3   | Phenol, 2-methoxy-                 | 20786142 | 13.081 |
| 4   | Phenol, 3-methyl-                  | 14679081 | 9.238  |
| 5   | Butyrolactone                      | 12460145 | 7.842  |
| 6   | Phenol, 2-methyl-                  | 11367011 | 7.154  |
| 7   | 2-Cyclopenten-1-one, 2,3-dimethyl- | 9003381  | 5.666  |
| 8   | 2(1H)-Pyridinone                   | 5920646  | 3.726  |
| 9   | Methenamine                        | 5587952  | 3.517  |
| 10  | Phenol, 4-ethyl-                   | 4661091  | 2.933  |

food-grade wood vinegar and separate the tar, wood vinegar was purified by distillation at 190°C. Wood vinegar compounds was analyzed using GC-MS (Gas Chromatography-Mass Spectrometry). The data of the 15 runs are presented in Table 5. The Design expert-12 software was applied to programmed the experiment design.

## Results and discussion

### GC-MS analysis

The GC-MS analysis of the wood vinegar from the pyrolysis at 300°C, 340°C, and 380°C as presented in Tables 2 to 4 detected the presence of 9, 14, and 11

**Table 5.** BBD design of the observation and predicted values for wood vinegar production from cacao pod shells.

| Run | Pyrolysis Temperature (°C) | Pyrolysis time (min) | Particle size (cm) | Wood vinegar production |                |
|-----|----------------------------|----------------------|--------------------|-------------------------|----------------|
|     |                            |                      |                    | Observation (%)         | Prediction (%) |
| 1   | 300                        | 50                   | 5                  | 36.68                   | 35.5           |
| 2   | 300                        | 100                  | 5                  | 34.43                   | 34.89          |
| 3   | 380                        | 50                   | 5                  | 32.44                   | 31.96          |
| 4   | 380                        | 100                  | 5                  | 41.17                   | 42.75          |
| 5   | 300                        | 75                   | 3                  | 38.17                   | 38.2           |
| 6   | 300                        | 75                   | 7                  | 32.14                   | 33.02          |
| 7   | 380                        | 75                   | 3                  | 38.92                   | 38.83          |
| 8   | 380                        | 75                   | 7                  | 37.92                   | 36.6           |
| 9   | 340                        | 50                   | 3                  | 31.69                   | 33.4           |
| 10  | 340                        | 50                   | 7                  | 30.19                   | 30.18          |
| 11  | 340                        | 100                  | 3                  | 39.32                   | 38.9           |
| 12  | 340                        | 100                  | 7                  | 36.93                   | 34.86          |
| 13  | 340                        | 75                   | 5                  | 36.43                   | 36.01          |
| 14  | 340                        | 75                   | 5                  | 35.68                   | 36.01          |
| 15  | 340                        | 75                   | 5                  | 36.18                   | 36.01          |

compounds respectively, which were dominated by phenol and its derivatives.

Tables 2 to 4 show that the main components of wood vinegar from the cacao pod shells pyrolyzed at 300°C, 340°C, and 380°C came from the pyrolysis of lignin compounds (phenol) amounting to 45.4%, 29.7%, and 33.6% respectively. This is because the cacao pod shells contain quite high lignin compounds (14–38.8%).<sup>4,24</sup> The figures are not much different from a study by Lu et al.,<sup>25</sup> that the main component of wood vinegar is phenol compounds. However, different results were reported by Oramahi et al.<sup>26</sup> in which wood vinegar from *Shorea pachyphylla* contains such chemical compounds as acid. Furthermore, Tables 2 to 4 show that no such harmful compounds as PAHs (Polycyclic Aromatic Hydrocarbons) including pyrene, perylene, benzo(a) anthracene, and benzo(a) pyrene were formed at each pyrolysis temperature. This was probably due to the distillation process which removed harmful compounds and separated the tar from the final product. PAHs have a high boiling point of <525°C so during the distillation process at 190°C, they did not evaporate but remained in the flask.<sup>27</sup>

### Optimizing the production of wood vinegar

To find out the best conditions for the combination of pyrolysis time (A), pyrolysis temperature (B), and particle size (C), this study chose the wood vinegar production (%) as a response variable to the independent variable. Experimental results and predictions of wood vinegar production from cacao pod shells are presented in Table 5.

Table 6 shows a higher significance level of the corresponding coefficient indicated by a lower p-value, where a p-value of less than 0.01 indicates that

**Table 6.** Regression coefficient in wood vinegar production (%).

| Factor                  | Coefficient |         |         |
|-------------------------|-------------|---------|---------|
|                         | Estimate    | F-value | p-value |
| Intercept               | 36.30       | 7.91    | 0.0051  |
| A-Pyrolysis times       | 1.83        | 14.26   | 0.0054  |
| B-Pyrolysis temperature | 1.13        | 5.45    | 0.0478  |
| C-Particle size         | −0.5850     | 1.46    | 0.2609  |
| AB                      | 2.75        | 16.11   | 0.0039  |
| AC                      | −1.78       | 6.79    | 0.0313  |
| BC                      | 1.26        | 3.38    | 0.1032  |

Note: Coefficient of variation (CV): 3.77%;  $R^2 = 0.86$ .

the corresponding coefficient is very significant and suitable for use in the regression model. The model that describes the relationship between wood vinegar production (%) and the research variables presented in Eq. (1) is quite satisfactory. This is indicated by the value of the predictive coefficient on the response variable (0.86) as shown in Table 6. The results show a relatively good value for predicting the response variable. If the value of  $R^2$  is close to 1, the model is stronger and the response prediction is better.<sup>28</sup> The greater the value of the coefficient of variation (CV) indicates that there is a high variation in the data around the mean value so that the reliability of the research results becomes lower.<sup>29</sup> The CV describes the accuracy of the data points around the mean value. The CV value is a dimensionless number so it can be used as a substitute for the standard deviation to compare model variations. Meanwhile, the low coefficient of variation (CV = 3.77%) means a very high level of precision, indicating the results were found to be correct<sup>30</sup> and the predicted value is closer to the actual value. Similarly, Kusuma et al.,<sup>31</sup> stated that a very low CV indicates a very high level of precision and accuracy in the results of the study. The results showed

**Table 7.** Analysis of variance (ANOVA).

| Source             | Sum of Squares | df       | F-value     | p-value       | Adjusted R <sup>2</sup> |                  |
|--------------------|----------------|----------|-------------|---------------|-------------------------|------------------|
| Mean vs Total      | 19767.53       | 1        |             |               |                         |                  |
| Linear vs Mean     | 39.61          | 3        | 2.26        | 0.1379        | 0.2132                  |                  |
| 2FI vs Linear      | <b>49.17</b>   | <b>3</b> | <b>8.76</b> | <b>0.0066</b> | <b>0.7476</b>           | <b>Suggested</b> |
| Quadratic vs 2FI   | 1.30           | 3        | 0.1592      | 0.9194        | 0.6313                  |                  |
| Cubic vs Quadratic | 13.37          | 3        | 30.56       | 0.0319        | 0.9803                  |                  |
| Residual           | 0.2917         | 2        |             |               |                         |                  |
| Total              | 19871.28       | 15       |             |               |                         |                  |

**Table 8.** The recommended operation for an optimized condition in producing wood vinegar.

| Number | Pyrolysis time | Pyrolysis temperature | Particle size | Production of wood vinegar | Desirability |                 |
|--------|----------------|-----------------------|---------------|----------------------------|--------------|-----------------|
| 1      | <b>100.000</b> | <b>353.000</b>        | <b>3.000</b>  | <b>41.268</b>              | <b>1.000</b> | <b>Selected</b> |
| 2      | 100.000        | 380.000               | 6.638         | 41.093                     | 0.992        |                 |
| 3      | 100.000        | 380.000               | 6.664         | 41.078                     | 0.990        |                 |
| 4      | 100.000        | 380.000               | 6.852         | 40.974                     | 0.979        |                 |
| 5      | 99.998         | 380.000               | 6.871         | 40.963                     | 0.978        |                 |
| 6      | 100.000        | 380.000               | 6.913         | 40.940                     | 0.976        |                 |
| 7      | 100.000        | 347.010               | 3.014         | 40.939                     | 0.976        |                 |
| 8      | 100.000        | 380.000               | 6.985         | 40.900                     | 0.972        |                 |
| 9      | 99.901         | 380.000               | 7.000         | 40.881                     | 0.970        |                 |
| 10     | 100.000        | 328.178               | 3.000         | 39.723                     | 0.847        |                 |
| 11     | 99.995         | 317.465               | 3.000         | 39.021                     | 0.773        |                 |
| 12     | 83.405         | 300.007               | 3.000         | 37.306                     | 0.592        |                 |
| 13     | 79.735         | 300.973               | 3.000         | 37.189                     | 0.580        |                 |
| 14     | 72.333         | 300.000               | 3.000         | 36.924                     | 0.552        |                 |

that the response equation resulted in a response model that was suitable for the BBD experiment.

The production of wood vinegar (Y) as a function of pyrolysis time (A), pyrolysis temperature (B), and wood particle size (C) can be approached by the following Eq. (1):

$$Y = 36.30 + 1.83A + 1.13B - 0.585C + 2.75AB - 1.78AC + 1.26BC. \quad (1)$$

The equation can be used to predict about wood vinegar production (%) with a certain value for each factor. Regression analysis is obtained from Eq. (1), where the yield of wood vinegar is described as a function of temperature and pyrolysis time ( $p < 0.05$ ). A positive (+) sign on the coefficient means that increasing these variables also increase the current response. Conversely, coefficients with a negative (−) sign suggest that raising these variables will cause the present response to decrease.<sup>32</sup>

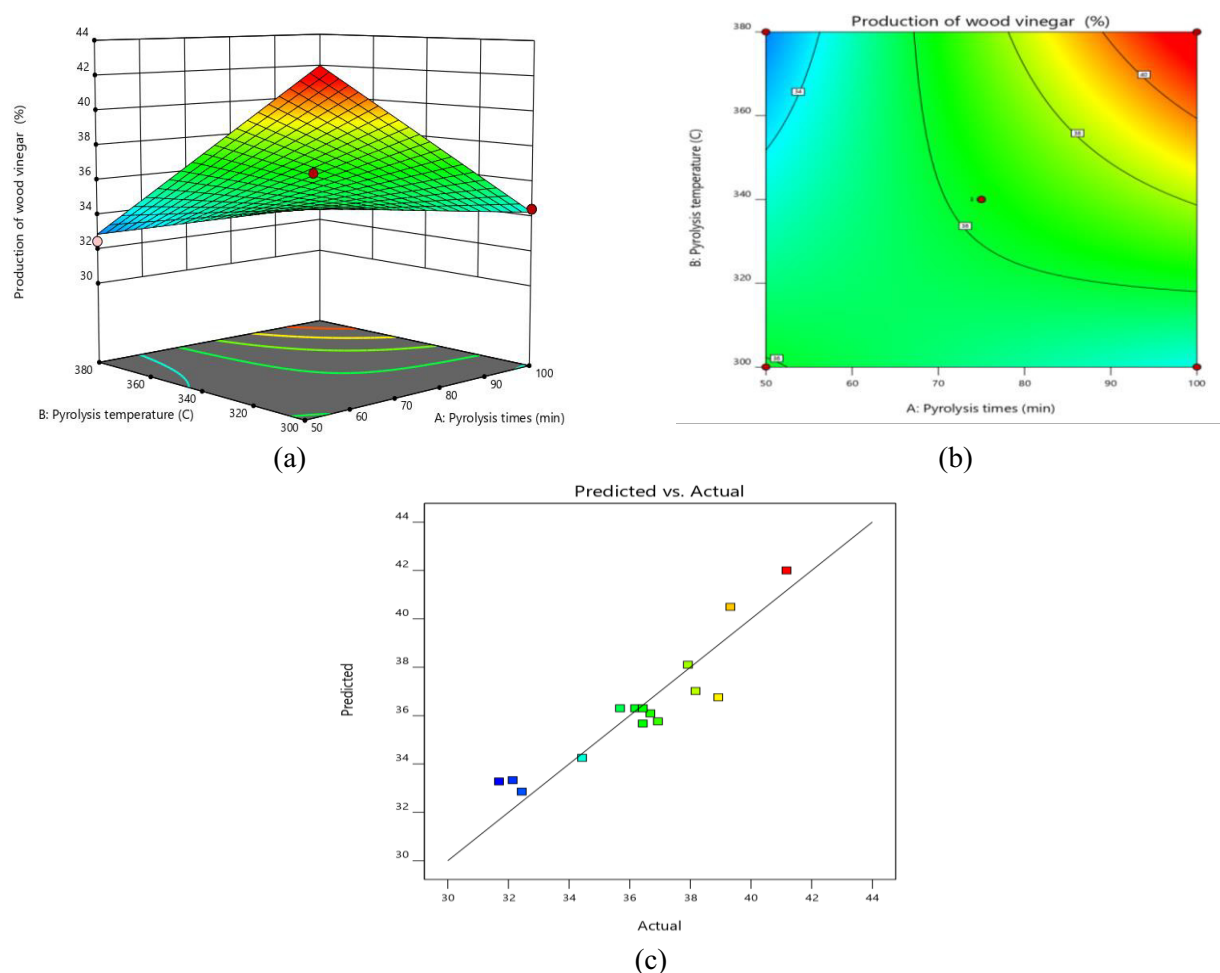
An analysis of variance (ANOVA) on the results of the 15 runs based on the three parameters is presented in Table 7. The effect of each independent variable is determined by the value of F and p. The greater the value of F and the smaller the value of P, the greater the effect of that variable on the response variable. From the ANOVA analysis in Table 7, the 2FI model has a very significant effect ( $p < 0.05$ ) while for the other models, it is not significant. The relatively

large F value ( $F = 8.76$ ) and very low probability value ( $P = 0.0066$ ) indicate that the model is very significant.<sup>33</sup> The model's suitability is also seen from the coefficient of determination ( $R^2 = 0.86$ ) which shows that 86% of the variability in the response can be explained by the model and only 14% of the total variation could not. To support the high significance of the model, the adjusted coefficient of variation ( $\text{Adj } R^2 = 0.7476$ ) is also quite high, which indicates a high relevance of the model. The  $R^2$  and  $\text{Adj-}R^2$  indicate a measure of the suitability of the experimental and predicted data on the model. The value of  $R^2 > 0.80$  indicates a high proportion of variability by the model and indicates a good agreement between the calculated and the observed results within the experimental range.<sup>34</sup>

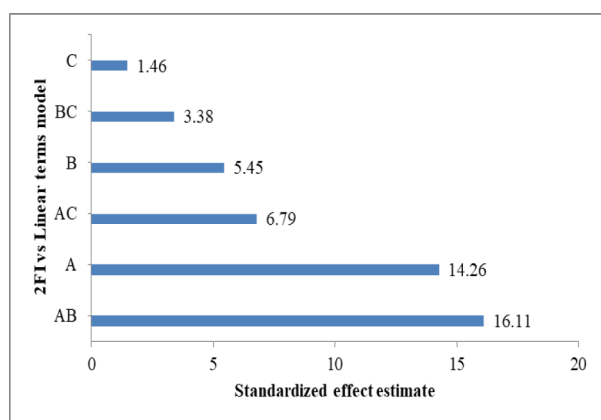
Numerical optimization was carried out to predict the optimum value of each variable in determining the most appropriate value in order to obtain the best wood vinegar production results. Experimental data were then compared with the results predicted by the model. The optimum condition was obtained at the pyrolysis time of 100 min, pyrolysis temperature of 353°C, and the particle size of 3 cm as shown in Table 8, with a desirability value of 1. The experimental results are not much different from the predicted value, that is, under such condition.

Fig. 1a shows the three-dimensional (3D) curve; 1(b) a contour plot illustrating the effect of variables including pyrolysis time (A) and pyrolysis





**Fig. 1.** (a). 3D response surface curve (b). Contour plots for production of wood vinegar showing the interaction between pyrolysis time (A, min) and pyrolysis temperature (B, °C), (c). Relationship between predicted vs actual production of wood vinegar.



**Fig. 2.** Pareto chart of the model.

temperature (B) on the response (wood vinegar production); and 1(c) the relationship between the predicted and the actual values. The percentage of wood vinegar produced ranged from 30.18%–42.75%. Wood vinegar has a maximum yield of

42.50%. At low temperatures, the production of wood vinegar is less, possibly because the contained compounds have not been completely decomposed. In other words, the low temperature was not sufficient in enabling the pyrolysis process to take place completely. The most influential factor in maximizing the production of wood vinegar is the pyrolysis temperature.<sup>20</sup> The Pareto chart in Fig. 2 demonstrates the effects of pyrolysis time, temperature, and particle size. The bar length in relation to reference line indicates the impact of each variable. Fig. 2 indicates that the wood vinegar production (%) was most affected by pyrolysis time and temperature (AB). The interaction between C, B and C, and B has little effect.

## Conclusion

RSM was carried out for the response of the wood vinegar yield. The results of the verification of the experimental response value are in a good range

with the predicted value. Optimization using the RSM method suggests that the optimum condition for wood vinegar production from cacao pod shells is at 3cm wood particle size, 352.8°C pyrolysis temperature, and 99.9 min pyrolysis time. Such operating conditions could yield the wood vinegar to 41.27%. The results of the GC-MS analysis show that phenol is the main component in the produced wood vinegar, while harmful compounds such as PAHs are not found. RSM could be a novel approach for optimizing wood vinegar production from cacao pod shells, particularly in terms of time and energy consumption during pyrolysis.

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## Authors' declaration

- Conflicts of Interest: None.
- We hereby confirm that all the Figures and Tables in the manuscript are ours. Furthermore, any Figures and images, that are not ours, have been included with the necessary permission for republication, which is attached to the manuscript.
- No animal studies are present in the manuscript.
- No human studies are present in the manuscript.
- No potentially identified images or data are present in the manuscript.
- Ethical Clearance: The project was approved by the local ethical committee at Universitas Syiah Kuala, Banda Aceh, Indonesia.

## Authors' contribution statement

H.D. and M.F. contributed to the design, conceptualization, and implementation of the research. H.D. experimented. M.F. contributed to supervision, validation, and writing review & editing. H.D, M.F, M., and S. performed RSM simulation and wrote the paper with input from all authors. M. and S. participated in data curation and writing review & editing.

## References

1. Sukorini H, Aigahayunindy FW, Septia ED, Khewkhom N. Exploration and effectiveness of trichoderma sp. From Jember and Trenggalek, East Java, Indonesia cacao plantation as a biological control of phytophthora palmivora. E3S Web Conf. 2021;226. <https://doi.org/10.1051/e3sconf/202122600022>.
2. Rojo-Poveda O, Barbosa-Pereira L, Zeppa G, Stévigny C. Cocoa bean shell—a by-product with nutritional properties and biofunctional potential. *Nutrients*. 2020;12(4):1123. <https://doi.org/10.3390/nu12041123>.
3. Rincón-Quintero AD, Del Portillo-Valdés LA, Cárdenas-Arias CG, Tarazona-Romero BE, Rondón-Romero WL, Durán-Sarmiento MA. A bibliometric analysis of the uses of the cocoa pod shell. *IOP Conf Ser Mater Sci Eng*. 2021;1154(1):012032. <https://doi.org/10.1088/1757-899X/1154/1/012032>.
4. Younes A, Karboune S, Liu L, Andreani ES, Dahman S. Extraction and characterization of cocoa bean shell cell wall polysaccharides. *Polymers*. 2023;15(3):745. <https://doi.org/10.3390/polym1503074>.
5. Djali M, Kayaputri IL, Kurniati D, Sukarminah E, Mudjenan IMH, Utama GL. Degradation of lignocelluloses cocoa shell (theobroma cacao L.) by various types of mould treatments. *J Food Qual*. 2021;2021:1–8. <https://doi.org/10.1155/2021/6127029>.
6. Sarmiento-Vásquez Z, Vandenbergh L, Rodrigues C, Tanobe VOA, Marín O, de Melo Pereira GV, *et al*. Cocoa pod husk valorization: Alkaline-enzymatic pre-treatment for propionic acid production. *Cellulose*. 2021;28:4009–4024. <https://doi.org/10.1007/s10570-021-03770-5>.
7. Oduro-Mensah D, Ocloo A, Nortey T, Antwi S, Okine LK, Adamafi NA. Nutritional value and safety of animal feed supplemented with talaromyces verruculosus-treated cocoa pod husks. *Sci Rep*. 2020;10(1):13163. <https://doi.org/10.1016/j.esd.2022.12.007>.
8. Dutra JDCF, Passos MF, García GJY, Gomes RF, Magalhães TA, dos Santos FA, *et al*. Anaerobic digestion using cocoa residues as substrate: systematic review and meta-analysis. *Energy Sustain Dev*. 2023;72:265–277. <https://doi.org/10.1016/j.esd.2022.12.007>.
9. Dahunsi SO, Adesulu-Dahunsi AT, Izebere JO. Cleaner energy through liquefaction of cocoa (theobroma cacao) pod husk: Pretreatment and process optimization. *J Clean Prod*. 2019;226:578–588. <https://doi.org/10.1016/j.jclepro.2019.04.112>.
10. Desvita H, Faisal M, Mahidin Suhendrayatna. Characteristic of liquid smoke produced from slow pyrolysis of cacao pod shells (Theobroma cacao L). *Int J GEOMATE*. 2021;20(80):17–22. <https://doi.org/10.21660/2021.80.6154>.
11. Anokye R, Boadu KB, Fianko CN, Amegashiti, VB. The chemical composition of Savannah bamboo (Oxytenanthera abyssinica) vinegar at varying pyrolysis temperatures and its termiticidal activity against wood-feeding termites. *Adv. Bamboo Sci*. 2024;6:1–7. <https://doi.org/10.1016/j.bamboo.2024.100063>.
12. Surboy MDC, Arundina I, Rahayu RP, Mansur D, Bramantoro T. Potential of distilled liquid smoke derived from coconut (Cocos nucifera L) shell for traumatic ulcer healing in diabetic Rats. *Eur J Dent*. 2019;13(02):271–279. <https://doi.org/10.1055/s-0039-1693527>.
13. Rahmasari Y, Yemiş GP. Characterization of ginger starch-based edible films incorporated with coconut shell liquid smoke by ultrasound treatment and application for ground beef. *Meat Sci*. 2022;188:108799. <https://doi.org/10.1016/j.meatsci.2022.108799>.
14. Chantanumat Y, Phetwarotai W, Sangthong S, Palamanit A, Abu Bakar MS, *et al*. Characterization of bio-oil and biochar from slow pyrolysis of oil palm plantation and palm oil mill wastes. *Biomass Convers Biorefin*. 2023;13(15):13813–13825. <https://doi.org/10.1007/s13399-021-02291-2>.

1. Sukorini H, Aigahayunindy FW, Septia ED, Khewkhom N. Exploration and effectiveness of trichoderma sp. From Jember and Trenggalek, East Java, Indonesia cacao plantation as a

15. Adiningsih Y, Priatni A. Characterization of rubber shell liquid smoke at various pyrolysis temperatures and the application to latex coagulant. In Joint Symposium on Tropical Studies, Atlantis Press, (JSTS-19). 2021;423–428. <https://doi.org/10.2991/absr.k.210408.070>.
16. Mansur D, Sugiwati S, Rizal WA, Suryani R, Maryana R. Pyrolysis of cajuput (melaleuca leucadendron) twigs and rice (oryza sativa) husks to produce liquid smoke-containing fine chemicals for antibacterial agent application. Biomass Convers Biorefin. 2023;13(12):10561–10574. <https://doi.org/10.1007/s13399-021-01896-x>.
17. Arundina I, Frimayanti N, Surboyo MD, Budhy TI, Iskandar B, Pradana A, et al. In silico study of liquid smoke rice husk against COVID-19. Eur J Dent. 2023;17(02):492–496. <https://doi.org/10.1055/s-0042-1750776>.
18. Triawan DA, Nasution AV, Sutanto TD, Nesbah N, Widiyati E, Adfa M, Banon C, Nurwidiyanti R. Preparation and characterization of liquid smoke from wood sawdust *Azadirachta excelsa* (Jack) M. jacobs and its application as a natural rubber coagulant. In IOP Conference Series: Earth and Environmental Science. 2022;1108(1):012052. <https://doi.org/10.1088/1755-1315/1108/1/012052>.
19. Oramahi HA, Yoshimura T, Rusmiyanto E, Kustiati K. Optimization and characterization of wood vinegar produced by shorea laevis ridl wood pyrolysis. Indones. J Chem. 2020;20(4):825–832. <https://doi.org/10.22146/ijc.45783>.
20. Xin X, Dell K, Udugama IA, Young BR, Baroutian S. Transforming biomass pyrolysis technologies to produce liquid smoke food flavouring. J Clean Prod. 2021;294:125368. <https://doi.org/10.1016/j.jclepro.2020.125368>.
21. Doti B, Nyaanga DM, Nyakach S, Nyaanga J. Optimization of pyrolysis parameters in production of pyroligneous acid from acacia twigs. J. Energy Environ. Chem Eng. 2022;8(1):1–13. <https://doi.org/10.37017/jeae-volume8-no1.2022-1>.
22. Ahmed AW, Atiya MA, M-Ridha MJ. Treatment of dairy wastewater by electrocoagulation using iron filings electrodes. Baghdad Sci J. 2023;20(3):1027–1027. <https://dx.doi.org/10.21123/bsj.2023.7987>.
23. Faisal M, Kamaruzzaman S, Desvita H, Annisa D, Zahara C. Response surface methodology for optimization of liquid smoke production yield from durian rinds (*Durio zibethinus* Murr.) Mater Today: Proceedings. 2023;87:187–191. <https://doi.org/10.1016/j.matpr.2023.02.395>.
24. Hougni DGJ, Schut AG, Woittiez LS, Vanlauwe B, Giller KE. How nutrient rich are decaying cocoa pod husks? The kinetics of nutrient leaching. Plant Soil. 2021;463:155–170. <https://doi.org/10.1007/s11104-021-04885-1>.
25. Lu X, Han T, Jiang J, Sun K, Sun Y, Yang W. Comprehensive insights into the influences of acid-base properties of chemical pretreatment reagents on biomass pyrolysis behavior and wood vinegar properties. J Anal Appl Pyrolysis. 2020;151:104907. <https://doi.org/10.1016/j.jaap.2020.104907>.
26. Oramahi HA, Wardoyo ERP. Optimization of liquid smoke from Shorea pachyphylla using response surface methodology and its characterization. Sci Technol Indones. 2022;7(2):257–262. <https://doi.org/10.26554/sti.2022.7.2.257-262>.
27. Xu L, Yu J, Wang W, Wan G, Lin L, et al. Upgrading and PAHs formation during used lubricant oil pyrolysis at different heating modes. J Anal Appl Pyrolysis. 2023;169:105813. <https://doi.org/10.1016/j.jaap.2022.105813>.
28. Pratap B, Mondal S, Rao, BH. Prediction of compressive strength of bauxite residue-based geopolymer mortar as pavement composite materials: an integrated ANN and RSM approach. Asian J Civ Eng. 2024;25(1):597–607. <https://doi.org/10.1007/s42107-023-00797-w>.
29. Mada T, Duraisamy R, Guesh F. Optimization and characterization of pectin extracted from banana and papaya mixed peels using response surface methodology. Food Sci Nutr. 2022;10(4):1222–1238. <https://doi.org/10.1002/fsn3.2754>.
30. Chouaibi M, Daoued KB, Riguane K, Rouissi T, Ferrari G. Production of bioethanol from pumpkin peel wastes: Comparison between response surface methodology (RSM) and artificial neural networks (ANN). Ind Crops Prod. 2020;155:112822. <https://doi.org/10.1016/j.indcrop.2020.112822>.
31. Kusuma HS, Amenaghawon AN, Darmokoesoemo H, Neolaka YA, Widyaningrum BA, Anyalewechi CL, et al. Evaluation of extract of ipomoea batatas leaves as a green coagulant-flocculant for turbid water treatment: Parametric modelling and optimization using response surface methodology and artificial neural networks. Environ Technol Innov. 2021;24:102005. <https://doi.org/10.1016/j.eti.2021.102005>.
32. Wyantuti S, Setyorini Z, Ishmayana S, Hartati Y, Firdaus M. Optimization of voltammetric determination of dysprosium (III) using plackett-burman and RSM-CCD experimental designs. Baghdad Sci J. 2020;17(4):1198–1198. <https://doi.org/10.21123/bsj.2020.17.4.1198>.
33. Andrade C. The P value and statistical significance: misunderstandings, explanations, challenges, and alternatives. Indian J Psychol Med. 2019;41(3):210–215. [https://doi.org/10.4103/IJPSYM.IJPSYM\\_193\\_19](https://doi.org/10.4103/IJPSYM.IJPSYM_193_19).
34. Rafiq W, Napih M, Habib N Z, Sutanto M H, Alaloul Wesam, Imran Khan Muhammad, et al. Modeling and design optimization of reclaimed asphalt pavement containing crude palm oil using response surface methodology. Constr Build Mater. 2021;291:123288. <https://doi.org/10.1016/j.conbuildmat.2021.123288>.



# تحسين الخل الخشبي من قشور قرون الكاكو من خلال منهجية الاستجابة السطحية

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## الخلاصة

الغرض من هذه الدراسة هو إيجاد الظروف المثلى لإنتاج خل الخشب من قشور ثمار الكاكو باستخدام منهجية الاستجابة السطحية (RSM).

تم استخدام Box Behnken Design (BBD) لتحسين متغيرات أوقات الانحلال الحراري ودرجة الحرارة وحجم الجسيمات. تم تحضير خل الخشب بتقنية الانحلال الحراري البطيء RSM. مع ثلاثة متغيرات للتصميم بما في ذلك مدة الانحلال الحراري عند 50 و 75 و 100 دقيقة؛ درجات حرارة الانحلال الحراري عند 300 درجة مئوية، و 340 درجة مئوية، و 380 درجة مئوية؛ وتم تطبيق حجم الجسيمات 3 و 5 و 7 سم مع 15 جولة.

تم إجراء التوصيف الكيميائي لخل الخشب عن طريق تحليل تحليل كروماتوغرافيا الغاز ومطياف الكتلة (GC-MS). أظهرت النتائج أن مركبات الفينول والفيوران والكيون كانت المكون الرئيسي في خل قشور الكاكو. تم تحديد الإنتاج الأمثل لخل الخشب من قشور قرون الكاكو بناءً على نتائج RSM في وقت انحلال حراري قدره 100 دقيقة، ودرجة حرارة 353 درجة مئوية، وحجم جسيم يبلغ 3 سم.

**الكلمات المفتاحية:** قشور قرون الكاكو، التحسين، الانحلال الحراري، RSM، خل الخشب.