

2006/9/17:

2008/6/5:

(Uniflow)

(Uniflow)

(20) (L/D)
(D=30,20,15 and 10mm)
($\theta = 30^\circ$)

(350mm) ($\theta = 1.72^\circ$)

(D=20mm, L=400mm)
(dc=12mm)
(Y=0.313) (2.4 C)
(Y=0.812) (47.5 C)
($T_i = 33^\circ \text{C}$)

($P_{iabs} = 2-6$)

(ise=24%) (D=20mm, L=400mm)
(Y) (COP=0.14) (Y=0.753) (η)

($P_{iabs} = 2-6$)

($\eta_e = 34\%$) (Y=0.704) ($Q_r = 1385 \text{ Watt}$)
(Y=0.323)

The effect of changing internal tube diameter on the performance of uniflow vortex tube

Abstract

In this present work, the optimum design and performance of the uniflow vortex tube used as a cooling and heating device of high efficiency is investigated experimentally. Great attempts to reach minimizing the uniflow vortex tube size with high separation energy are investigated.

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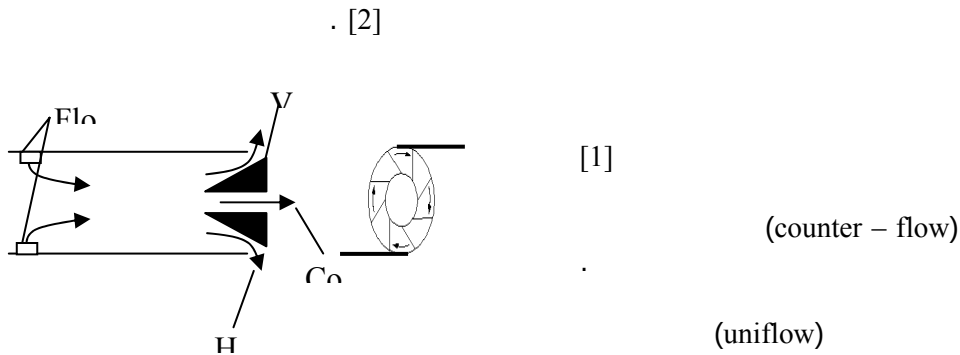
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The experimental investigation was carried out on a vortex tube rig especially designed for the present study covering all tests. Experiments were carried out on the vortex tube by fixing (L/D) at (20) for five tubes ,four of them are straight with diameters (30,20,15and 10) and the last is diverge tube with angle($\theta=1.72^\circ$) and length(350mm),the cone angle is ($\theta= 30^\circ$),consequently the study of the energy separation performance of five uniflow vortex tubes wer carried out.

The experimental results shows that the pronounced influence of the uniflow vortex tube ($D=20\text{mm}$, $L=400\text{mm}$) on the energy separation performance at cone valve diameter ($d_c=12\text{mm}$), i.e the highest temperature of the hot air stream and the lowest temperature. The cold air stream reaches (47.5C°) at ($Y=0.812$) & (2.4C°) at ($Y=0.313$) respectively at the inlet air temperature ($T_i=33\text{C}^\circ$).

The results of the uniflow vortex tube shows that increasing the isentropic efficiency & coefficient of performance with increasing inlet air pressure within the range ($P_{i_{abs}} = 2\text{-}6\text{ bar}$) which reaches $\eta_{ise} = 24\%$ at $Y=0.753$ & $\text{COP}=0.14$ at the same Y . Also the result shows that refrigeration capacity & efficiency of the energy separation increasing with increase inlet air pressure & reaches $Q_r=1385\text{ watt}$ at $Y=0.704$ & $\eta_e = 34\%$ at $Y=0.323$.

شكل (1) أنبوب دوامي
ذو جريان باتجاه واحد (Uniflow)



(1947)
[3] (Hilsch)

(Nozzles)
(0.6D) (0.45D)

(1)

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- (shear work) [4] (Lay) (1959) (O.25D (50 D)
- (swirl) $\mathcal{E}r$ (38Kpa) (238Kpa)
- : equation) (Z)
- $\rho u \frac{\partial v}{\partial r} + \frac{\rho uv}{r} =$ (0.8R)
- $\rho \mathcal{E}r \left[\frac{\partial^2 v}{\partial r^2} + \frac{1}{r} \frac{\partial v}{\partial r} - \frac{v}{r^2} \right] \dots (1)$
- (25) [6] (Gulyaev) (1966)
- (20,15,10.8,7.5mm)
- (15-80) (13)
- (2-6bar) (Lemesh and (1983)
- (Y=0-1) [7] Scenchuk)
- (12)
- (Ranque-Hilsch)
- (1) (D_n=4mm) (290 and 480K)
- (D=7.5-20mm) (30) (0.4D) (orifice)
- (L/D=20) (D=30mm)
- (3) (Al-Omran) (2002) [8]
- (I,C,H)
- $m_i h_i = m_c h_c + m_h h_h \dots (3)$
- $m_i = m_c + m_h \dots (2)$
- $Y = \frac{\Delta T_h}{\Delta T_h + \Delta T_c} \dots (6)$
- $(T_i - T_c) = m_h (T_h - T_i) = m_i - m_c (T_h - T_i) \dots (4)$
- or
- $Y = \frac{m_c}{m_i} \dots (5)$
- (P_a) (P_i)
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- \ **
- \ ***

$$\Delta T_{c'} = T_i - T_{c'} = T_i \left[1 - \left(\frac{P_a}{P_i} \right)^{\frac{\gamma-1}{\gamma}} \right] \quad \dots (7)$$

$$(\Delta T_c)$$

$$(\Delta T_c)$$

$$\Phi = \Delta T_{rel} = \frac{\Delta T_c}{T_{c'}} \quad \dots (8)$$

$$\zeta_{ise} = Y \Delta T_{rel} \quad \dots (8.a)$$

$$\eta_{ise} = \dots$$

[9]

$$\left(\frac{P_i}{P_a} \right)^{\frac{\gamma-1}{\gamma}} T_f = T_i \quad \dots (10)$$

$$W_{act} = \frac{m_i c_p T_i \left\{ \left(\frac{P_i}{P_a} \right)^{\frac{\gamma-1}{\gamma}} - 1 \right\}}{\eta_{comp}} \quad \dots (11)$$

$$(T_i)$$

$$T_c \Delta Q_r = m_c C_p \quad \dots (12)$$

$$T_i = \frac{\Delta T_{c'}}{1 - \left(\frac{P_a}{P_i} \right)^{\frac{\gamma-1}{\gamma}}} \quad \dots (14)$$

$$\phi \eta_{ise} \left(\frac{P_a}{P_i} \right)^{\frac{\gamma-1}{\gamma}} \quad COP=Y$$

$$(COP)$$

$$\frac{(P_i)}{(T_i - T_f)} = \frac{(P_a)}{(T_i - T_f)} \quad [10] :$$

$$W_{act} = \frac{m_i c_p (T_f - T_i)}{\eta_{comp}} \quad \dots (9)$$

$$\eta_{comp} \quad (10)$$

$$COP = \frac{m_c C_p \Delta T_c \eta_{comp}}{M_{iCpTi} \left\{ \left(\frac{P_i}{P_a} \right)^{\frac{\gamma-1}{\gamma}} - 1 \right\}} \quad \dots (13)$$

$$(9) \quad (T_i) \quad (13)$$

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..(15)

$$\frac{\Delta T_c}{\Delta T_c^-} \eta_{comp} \left(\frac{P_a}{P^i} \right)^{\frac{\gamma-1}{\gamma}} \text{COP}$$

-3

($T_c \Delta$)
(2-6)

(bar

: (3)

(L\D=20) (1)
(dc=12mm)

(glass wool)

: - a

(dc=12mm) (1)
 $P_{iabs} =$

(40mm)

(10mm)

($T_h \Delta$) (2bar

(Nozzle)

($\Delta T_h = 6.5^\circ C$)

(Y=0.8)

.($Y \approx 1$) ($\Delta T_h = 0.9^\circ C$)

. (swirl flow)

-(1)

- B

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Clindrical-Squared (

Housing

($\Delta T_c = -14.6^\circ C$)

(Y=0.313)

∴

C

($Y \approx 1$) ($\Delta T_c = -0.2^\circ C$)

(Nozzle)

-:

($P_{iabs} = 6\text{bar}$)

. (Swirl flow)

∴ 2,3,4

- e

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(Y=0.841) ($\Delta T_h = 13.5^\circ C$)

-4

-1

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.(Y=0.313) ($\Delta T_c = -26.5^\circ C$)

(Y)

($T_c \Delta$)

(Y)

(Y=0.3-0.4)

.(Y)

(4)

(Y)

:(L/D)

(ΔT_h)

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- 4 :
- (COP)
(14)
- (Y =0.5-0.7)
(Y) (33C
- (Y=0.964)
(2)
(Y=0.77) (COP=0.14)
(4)
(COP=0.09) (dc=8mm)
(Y=0.58)
- 5 :
- (11)
Y=0.6-)
(T_i= 33C)
(ΔT_c) (Y)
(Y=0.986)
- (8)
(1)
(P_{iabs}=6bar)
(dc=12mm)
- (Y)
(0.5 0.7)
T_i=33C)
(ΔT_c) (Y)
(Y=0.964)
- (7)
(Y)
(1)
P_{iabs}=6bar)
(dc=12mm
(dc=14mm)
(dc=12mm)
- (Y=0.62) (Q_r=1100watt)
(ΔT_h = -30.6°C)
(Y= 0.313)
- (ΔT_h = 14.5°C)
(Y=0.823)
- 3
- (ΔT_h)
(Y)
(Y=0.8-0.9)
- (6 5)
(L/D)
(ΔT_c) (ΔT_h)
(Y=0. 313)
Y=0.812)
(6 bar)
(33C)
(L/D=20)
- 3
:
(8.a)
(Y)
(0.5 0.7)
T_i=33C)
(ΔT_c) (Y)
(Y=0.964)
(7)
(Y)
(1)
P_{iabs}=6bar)
(dc=12mm
(dc=14mm)
(dc=12mm)
(Y=0.55) (η_{ise} = 21.8%)
(1)
-5
-1
(dn=6.5mm)
(N=2) (dc=12mm)
(L/D=20) (30)
(2)
(D=20mm,L=400mm)
(dc=12mm
2
*
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(dc=12mm
(P_{iabs}=6bar)

(COP)

($\eta_{ise} = 24\%$)

.(Y=0.724) (COP=0.14)

(Y)

(0.6-0.8)

(dc=12mm)

(2)

(Pi=6bar)

(Q_r=1380 Watt)

. (Y=0.704)

(Y ≈ 1)

(ΔT_c)

(Y)

(Y=0.3-0.4)

. (Y)

Y=0.5-)

(Y)

(0.7

. [8]

(2)

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(1)

6- Reference:

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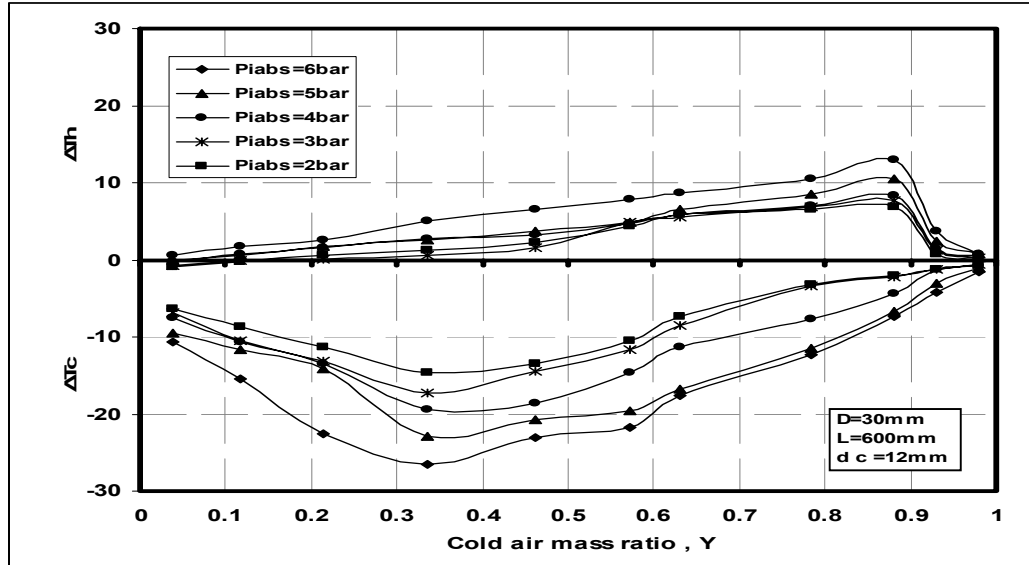
Chamber	Dmm	L/D	Lmm	Dn mm	Dc mm	Dh mm
Vortex tube No. 1	30	20	600	6.5	6	14
					8	
					10	22
					12	
					14	28
Vortex tube No. 2	20	20	400	6.5	6	14
					8	
					10	22
					12	
					14	28
Vortex tube No. 3	15	20	300	6.5	6	14
					8	22
					10	
					12	28
Vortex tube No. 4	10	20	200	6.5	8	
					6	
Vortex tube No. 5 Taper	30 20	20	350	6.5	6	14
					8	22
					10	28
					12	28
					14	

(1)

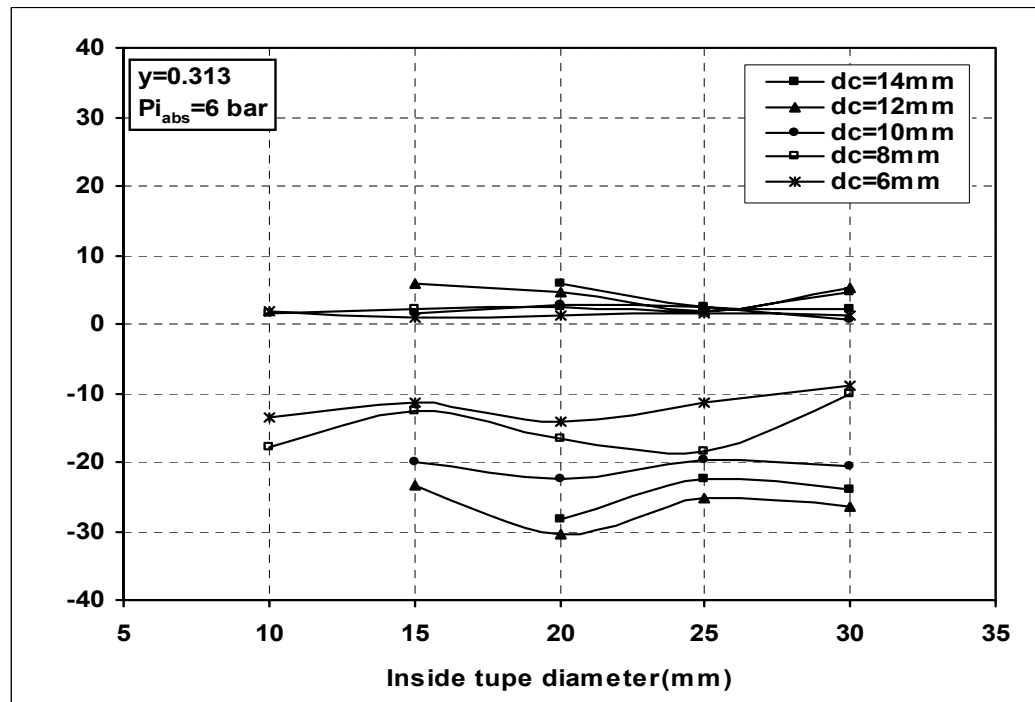
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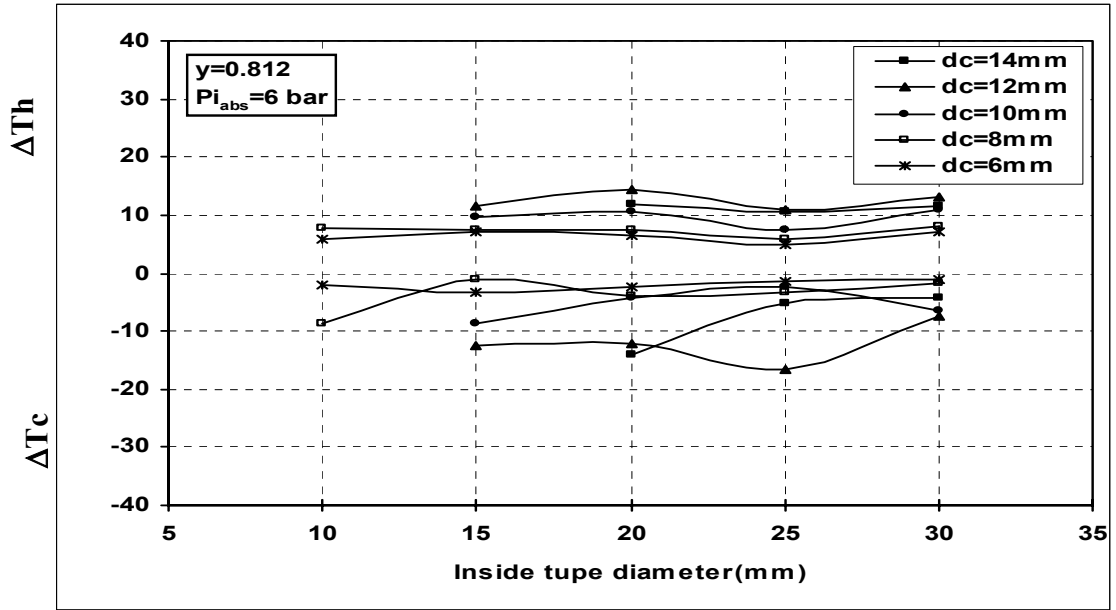
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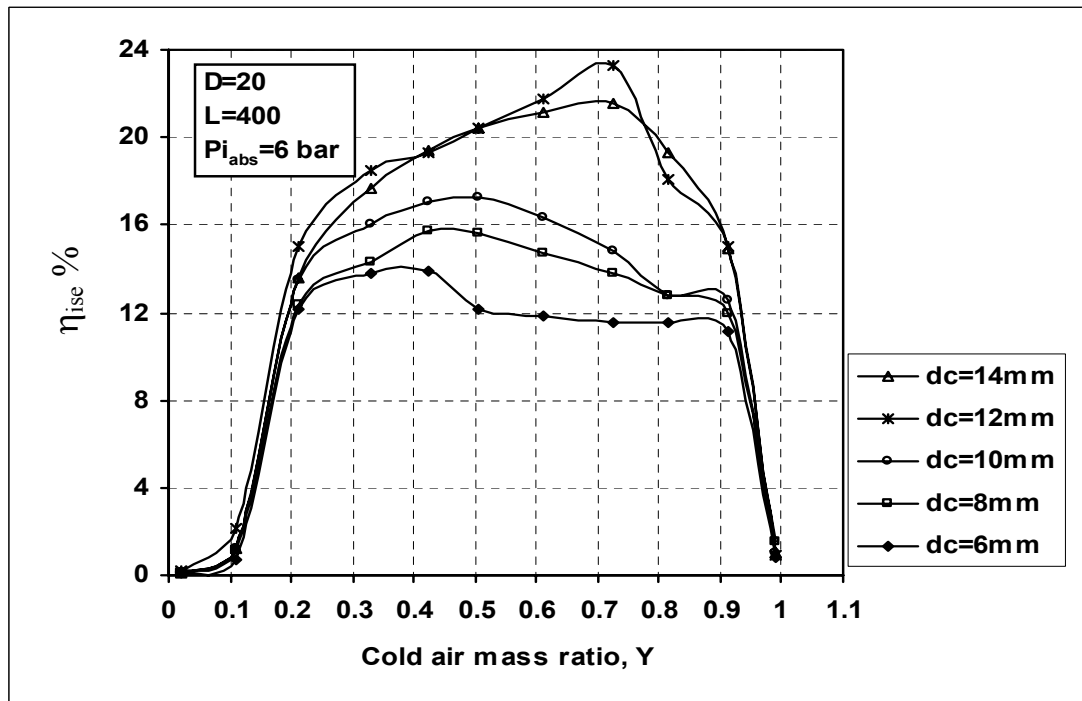
شكل (4) يمثل العلاقة بين نسبة كتلة الهواء البارد والفارق الحراري بين درجة حرارة الهواء الداخل وكل من درجة حرارة الهواء البارد والساخن للأنبوب الدوامي رقم (1) ولمختلف ضغوط الهواء الداخل (P_i)



شكل (5) يمثل العلاقة بين القطر الداخلي للأنبوب الدوامي والفارق الحراري بين درجة حرارة الهواء الداخل وكل من درجة حرارة الهواء البارد والساخن ولجميع أقطار الصمام المخروطي ولضغط الهواء الداخل ($P_i=6\text{bar}$) ونسبة كتلة الهواء البارد ($Y=0.313$)

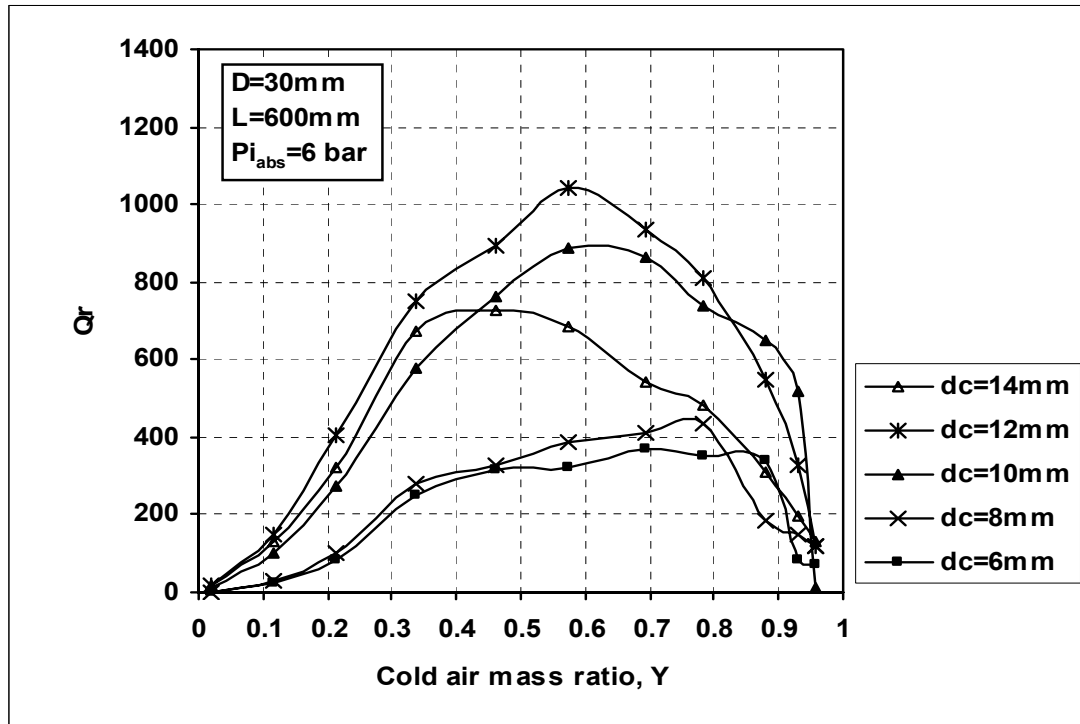


شكل (6) يمثل العلاقة بين القطر الداخلي للانبوب الدوامي والفارق الحراري بين درجة حرارة الهواء الداخل وكل من درجة حرارة الهواء البارد والساخن ولجميع اقطار الصمام المخروطي ولضغط الهواء الداخل ($P_i=6\text{bar}$) ونسبة كتلة الهواء البارد ($Y=0.812$)



شكل (7) يمثل العلاقة بين نسبة كتلة الهواء البارد والكفاءة الايزونتروبية للانبوب الدوامي رقم (1) ولجميع اقطار الصمام المخروطي ولضغط الهواء الداخل ($P_i=6\text{bar}$)

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شكل (8) يمثل العلاقة بين نسبة كتلة الهواء البارد وسعة التبريد للانبوب الدوامي رقم (1) ولجميع اقطار الصمام المخروطي ولضغط الهواء الداخل ($P_i=6\text{bar}$)

